# Thermocapillary convection in a cylindrical liquid-metal floating zone with a strong axial magnetic field and with a non-axisymmetric heat flux 

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This paper treats the steady three-dimensional thermocapillary convection in a cylindrical liquid-metal zone between the isothermal ends of two coaxial solid cylinders and surrounded by an atmosphere. There is a uniform steady magnetic field which is parallel to the common centrelines of the liquid zone and solid cylinders, and there is a non-axisymmetric heat flux into the liquid's free surface. The magnetic field is sufficiently strong that inertial effects and convective heat transfer are negligible, and that viscous effects are confined to thin boundary layers adjacent to the free surface and to the liquid-solid interfaces. With an axisymmetric heat flux, the axisymmetric thermocapillary convection is confined to the thin layer adjacent to the free surface, but with a non-axisymmetric heat flux, there is an azimuthal flow inside the free-surface layer from the hot spot to the cold spot with the circulation completed by flow across the inviscid central core region. This problem is related to the magnetic damping of thermocapillary convection for the floating-zone growth of semiconductor crystals in Space.

## 1. Introduction

In the floating-zone process, a semiconductor crystal is grown from a volume of liquid (melt) which is held by surface tension between the growing cylindrical single crystal and the coaxial melting polycrystalline feed rod. A heat flux into the free surface keeps the melt temperature above the solidification temperature $T_{s}$. On Earth, only small-diameter crystals can be grown by the floating-zone process because surface tension can only balance the hydrostatic pressure variation for small zones (Coriell \& Cordes 1977). With the heat flux provided by a single-loop radio-frequency induction coil around the melt, the electromagnetic (EM) body force in the skin-depth layer adjacent to the free surface augments the surface tension, so that larger crystals can be grown on Earth (Lie, Walker \& Riahi 1990). However, this EM force also drives a strong circulation in the melt, leading to spatial oscillations in the crystal's dopant concentration, called striations (Muhlbauer, Erdmann \& Keller 1983), where the dopant is added to give the semiconductor crystal the electrical properties needed for the integrated circuits to be manufactured on wafers sliced from the crystal. In an

Earth-orbiting vehicle, the residual acceleration is four or five orders of magnitude smaller than terrestrial gravity, so that large semiconductor crystals can be grown by the floating-zone process with nothing to augment the surface tension. The principal alternative for crystal growth in space is the Bridgman process in which the melt crystallizes inside a cylindrical ampoule, but stresses between the ampoule wall and the shrinking crystal can lead to surface dislocations in the crystal.

Since the surface tension of a liquid semiconductor decreases as the temperature is increased, surface-tension gradients drive a thermocapillary convection adjacent to the free surface from higher to lower temperatures. For the floating-zone growth of silicon or gallium-arsenide, the thermocapillary convection is periodic with temperature differences along the free surface of more than a few degrees Kelvin (Rupp et al. 1991), and this flow periodicity also produces the undesirable striations in the crystal. Numerical simulations (Muller \& Rupp 1991; Rupp et al. 1991) and experiments (Croll, Dold \& Benz 1994; Robertson \& O’Connor 1986) have shown that a strong steady uniform axial magnetic field can eliminate or greatly reduce the unsteadiness in the thermocapillary convection and the resultant striations in the crystal for the temperature differences along the free surface of 10 to 30 K which occur in the actual process.

The furnace used for floating-zone crystal growth in space is an ellipsoid with a 1 kW lamp at one focal point and with the molten floating zone at the other focal point, so that the focused optical heating from the lamp keeps the temperature in the melt above $T_{s}$ (Rupp et al. 1991). All previous treatments, including our studies (Morthland \& Walker 1996, 1997), of thermocapillary convection in the floating-zone process with optical heating and with or without a steady magnetic field have assumed that the heat flux into the free surface is axisymmetric. In reality, the optical heat flux is never axisymmetric because the lamp may not be exactly at the focal point, the lamp itself is not axisymmetric, the axis of the crystal, feed rod and zone may not be perfectly aligned with the major axis of the ellipsoid, and an observation window has a much lower reflectivity than the metal surface so it produces a cold spot at its azimuthal position. Without a magnetic field, the relative deviation from axisymmetry in the melt motion is probably comparable to that in the heat flux. However, an axial magnetic field strongly suppresses an axisymmetric motion because there is very little electrical resistance to the azimuthal electric currents needed to provide the EM flow suppression, but an axial field only weakly suppresses azimuthal velocities near the free surface because the electrically insulating atmosphere blocks the radial electric currents needed for the EM body force opposing this velocity (Ma \& Walker 1995). Therefore, with a strong axial magnetic field, a small deviation from axisymmetry in the heat flux can lead to a large deviation from axisymmetry in the melt motion. The results presented in this paper show that a deviation from axisymmetry leads to a fundamental change in the character of the flow. With an axisymmetric heat flux, the thermocapillary convection is confined to a boundary layer with an $O\left(\mathrm{Ha}^{-1 / 2}\right)$ dimensionless thickness adjacent to the free surface, where $H a=B L(\sigma / \mu)^{1 / 2}$ is the large Hartmann number, $B$ is the magnetic flux density of the externally applied steady uniform axial magnetic field and $L$ is half the axial length of the free surface from the crystal to the feed rod, while $\sigma$ and $\mu$ are the electrical conductivity and viscosity of the melt. In the rest of the melt, the velocity is zero to all orders in $H a$. With a non-axisymmetric heat flux, there are large $O\left(\mathrm{Ha}^{1 / 2}\right)$ velocities in the free-surface layer from the hottest to the coldest azimuthal positions, while the circulation is completed by an $O(1)$ velocity across the central inviscid core region.

## 2. Problem formulation

The appropriate characteristic velocity for electromagnetically suppressed thermocapillary convection is $U=q\left(-\mathrm{d} \gamma / \mathrm{d} T^{*}\right) / B k(\sigma \mu)^{1 / 2}$, where $q$ is the characteristic magnitude of the heat flux into the free surface, $\mathrm{d} \gamma / \mathrm{d} T^{*}$ is the constant negative gradient of the surface tension $\gamma$ with respect to the dimensional temperature $T^{*}$, and $k$ is the melt's thermal conductivity (Khine \& Walker 1994). In addition to the applied steady uniform axial magnetic field produced by a solenoid around the ellipsoidal furnace, there are 'induced' magnetic fields produced by the electric currents in the melt. The characteristic ratio of the induced to applied magnetic field strengths is the magnetic Reynolds number, $R_{m}=\mu_{p} \sigma U L$, where $\mu_{p}$ is the melt's magnetic permeability. Since $R_{m}$ is very small for all crystal-growth processes, the induced magnetic fields are negligible. Therefore, the magnetic field normalized by $B$ is simply $\hat{z}$, where $\hat{\boldsymbol{r}}, \hat{\theta}, \hat{z}$ are unit vectors for cylindrical coordinates with the $z$-axis along the common centrelines of the liquid zone and solid cylinders and with the origin midway between the ends of the cylinders.

The characteristic ratio of convective heat transfer to thermal conduction is the Péclet number, $P e=\rho c_{h} U L / k$, where $\rho$ and $c_{h}$ are the melt's density and specific heat. With a sufficiently strong magnetic field $U$ is small enough that $P e \ll 1$ (Morthland \& Walker 1997). Then the deviation of $T^{*}$ from $T_{s}$, normalized by $q L / k$, is $T(r, \theta, z)$ which is governed by $\nabla^{2} T=0$. In the Navier-Stokes equation, the characteristic ratio of the EM body force term to the inertial terms is the interaction parameter, $N=\sigma B^{2} L / \rho U$, which varies as $B^{3}$ for our $U$. Since our solution involves large, $O\left(H a^{1 / 2}\right)$, dimensionless velocities in a free-surface layer with an $O\left(\mathrm{Ha}^{-1 / 2}\right)$ dimensionless thickness, $N$ must be much larger than $H a^{3 / 2}$ in order to neglect inertial effects (Walker, Ludford \& Hunt 1972). With these assumptions, the dimensionless governing equations are

$$
\begin{array}{ll}
0=-\boldsymbol{\nabla} p+\boldsymbol{j} \times \hat{z}+H a^{-2} \nabla^{2} \boldsymbol{v}, & \boldsymbol{\nabla} \cdot \boldsymbol{v}=0 \\
\boldsymbol{j}=-\boldsymbol{\nabla} \phi+\boldsymbol{v} \times \hat{\boldsymbol{z}}, & \boldsymbol{\nabla} \cdot \boldsymbol{j}=0 \tag{1c,d}
\end{array}
$$

where $p, \boldsymbol{j}, \boldsymbol{v}$ and $\phi$ are the pressure, electric current density, velocity and electric potential function (voltage), normalized by $\sigma U B^{2} L, \sigma U B, U$ and $U B L$, respectively.

We neglect the small electrical conductivity of the feed rod and crystal, so that the boundary conditions at the liquid-solid interfaces are

$$
\begin{equation*}
\boldsymbol{v}=0, \quad j_{z}=0 \quad \text { at } \quad z= \pm 1 \tag{2}
\end{equation*}
$$

For terrestrial floating-zone crystal growth, the free surface is far from cylindrical because surface tension must balance the hydrostatic pressure variation (Coriell \& Cordes 1977). In Space, with a negligible hydrostatic pressure variation due to the small residual acceleration, the free-surface shape is very close to a cylinder (Morthland \& Walker 1996), and the free-surface distortion produced by the pressure variation associated with the melt motion is negligible (Lie et al. 1990). Therefore the boundary conditions at the free surface are

$$
\begin{align*}
v_{r} & =0, \quad \frac{\partial v_{\theta}}{\partial r}-\frac{v_{\theta}}{a}=-\frac{H a}{a} \frac{\partial T}{\partial \theta}  \tag{3a,b}\\
\frac{\partial v_{z}}{\partial r} & =-H a \frac{\partial T}{\partial z}, \quad j_{r}=0 \quad \text { at } \quad r=a \tag{3c,d}
\end{align*}
$$

where $a$ is the ratio of the floating zone's diameter to its axial length $2 L$. If the heat flux into the free surface is symmetric about the $z=0$ plane, then the melt motion is too,


Figure 1. Subregions of the liquid zone for $H a \gg 1$ and for $z>0$ : $\mathrm{c}=$ inviscid core region, $\mathrm{h}=$ Hartmann layer, $\mathrm{f}=$ free-surface layer, $\mathrm{i}=$ intersection region and $\mathrm{cr}=$ corner region.
so that we need only solve for $0 \leqslant z \leqslant 1$, with appropriate symmetry conditions at $z=0$. We make $p$ and $\phi$ unique by setting $p=\phi=0$ at $r=z=0$.

For $H a \gg 1$, the liquid zone can be divided into the subregions shown in figure 1. The Hartmann-layer solution satisfies (2) and matches the core solution, provided the latter satisfies the Hartmann conditions

$$
\begin{align*}
& v_{z c}=-H a^{-1} r^{-1}\left[\frac{\partial}{\partial r}\left(r v_{r c}\right)+\frac{\partial v_{\theta c}}{\partial \theta}\right],  \tag{4a}\\
& j_{z c}=H a^{-1} r^{-1}\left[\frac{\partial v_{r c}}{\partial \theta}-\frac{\partial}{\partial r}\left(r v_{\theta c}\right)\right] \text { at } z=1, \tag{4b}
\end{align*}
$$

neglecting $O\left(\mathrm{Ha}^{-2}\right)$ terms (Walker et al. 1972), where the subscript $c$ denotes a core variable. The solution of (1) which satisfies (4) is

$$
\begin{align*}
& j_{r c}=-\frac{1}{r} \frac{\partial p_{c}}{\partial \theta}, \quad j_{\theta c}=\frac{\partial p_{c}}{\partial r}, \quad j_{z c}=0,  \tag{5a-c}\\
& v_{r c}=-\frac{1}{r} \frac{\partial \phi_{c}}{\partial \theta}-\frac{\partial p_{c}}{\partial r}, \quad v_{z c}=0,  \tag{5d,e}\\
& v_{\theta c}=\frac{\partial \phi_{c}}{\partial r}-\frac{1}{r} \frac{\partial p_{c}}{\partial \theta}, \tag{5f}
\end{align*}
$$

neglecting $O\left(H a^{-1}\right)$ terms, where $p_{c}(r, \theta)$ and $\phi_{c}(r, \theta)$ satisfy $\nabla^{2} p_{c}=\nabla^{2} \phi_{c}=0$. In the present problem, the $O\left(\mathrm{Ha}^{-1}\right)$ term on the right-hand side of (4b) is needed in order to determine the equation governing the $O(1) \phi_{c}$ (Hunt \& Ludford 1968), while the $O\left(\mathrm{Ha}^{-1}\right)$ term on the right-hand side of (4a) plays no role. In other applications, the $O\left(H a^{-1}\right)$ term on the right-hand side of (4a) plays the key role when the Hartmann-
layer pumping drives the core flow (Hall \& Walker 1993). The boundary conditions on $p_{c}$ and $\phi_{c}$ at $r=a$ are obtained by matching the free-surface-layer solution, while $p_{c}=\phi_{c}=0$ at $r=0$.

For the free-surface layer, we stretch the local radial coordinate by introducing $\xi=H a^{1 / 2}(r-a)$. With the subscript $f$ denoting the leading-order term in the asymptotic expansion of a free-surface-layer variable then: $v_{\theta f}$ and $v_{z f}$ are $O\left(H a^{1 / 2}\right) ; v_{r f}, j_{\theta f}, j_{z f}$ and $\phi_{f}$ are $O(1) ; j_{r f}, p_{f}$ and an integration function $F_{f}$ are $O\left(\mathrm{Ha}^{-1 / 2}\right)$. The leading-order terms in (1) give expressions for the other variables in terms of $\phi_{f}$ and $F_{f}$, and give the equations governing $\phi_{f}$ and $F_{f}$ :

$$
\begin{align*}
v_{r f} & =-\frac{1}{a} \frac{\partial \phi_{f}}{\partial \theta}-\frac{\partial^{2} F_{f}}{\partial \xi \partial z}, \quad v_{\theta f}=\frac{\partial \phi_{f}}{\partial \xi}  \tag{6a,b}\\
j_{r f} & =\frac{\partial^{3} \phi_{f}}{\partial \xi^{3}}-\frac{1}{a} \frac{\partial^{2} F_{f}}{\partial \theta \partial z}, \quad j_{\theta f}=\frac{\partial^{2} F_{f}}{\partial \xi \partial z}  \tag{6c,d}\\
v_{z f} & =\frac{\partial^{2} F_{f}}{\partial \xi^{2}}, \quad j_{z f}=-\frac{\partial \phi_{f}}{\partial z}, \quad p_{f}=\frac{\partial F_{f}}{\partial z}  \tag{6e-g}\\
\frac{\partial^{2} \phi_{f}}{\partial z^{2}} & =\frac{\partial^{4} \phi_{f}}{\partial \xi^{4}}, \quad \frac{\partial^{2} F_{f}}{\partial z^{2}}=\frac{\partial^{4} F_{f}}{\partial \xi^{4}} \tag{6h,i}
\end{align*}
$$

The free-surface conditions (3) become

$$
\begin{align*}
\frac{\partial^{2} \phi_{f}}{\partial \xi^{2}} & =-\frac{1}{a} \frac{\partial T}{\partial \theta}(a, \theta, z), \quad \frac{\partial^{3} F_{f}}{\partial \xi^{3}}=-\frac{\partial T}{\partial z}(a, \theta, z),  \tag{7a,b}\\
\frac{\partial^{2} F_{f}}{\partial \xi \partial z}+\frac{1}{a} \frac{\partial \phi_{f}}{\partial \theta} & =0, \quad \frac{\partial^{3} \phi_{f}}{\partial \xi^{3}}-\frac{1}{a} \frac{\partial^{2} F_{f}}{\partial \theta \partial z}=0 \quad \text { at } \quad \xi=0 \tag{7c,d}
\end{align*}
$$

The intersection-region solution satisfies (2) and matches the free-surface-layer solution, provided the latter satisfies the Hartmann conditions (Walker et al. 1972)

$$
\begin{equation*}
\frac{\partial^{2} F_{f}}{\partial \xi^{2}}=0, \quad \frac{\partial \phi_{f}}{\partial z}=\frac{\partial^{2} \phi_{f}}{\partial \xi^{2}} \quad \text { at } \quad z=1 \tag{8a,b}
\end{equation*}
$$

Since the free-surface-layer pressure is $O\left(H a^{-1 / 2}\right)$, the $O(1)$ core pressure is zero at $r=a$, so that it is zero everywhere. With the subscript $c$ denoting the leading-order term in the asymptotic expansion of a core variable, $v_{r c}, v_{\theta c}$ and $\phi_{c}$ are $O(1)$, while $j_{r c}$, $j_{\theta c}$ and $p_{c}$ are $O\left(H a^{-1 / 2}\right)$, and the terms with $p_{c}$ in $(5 d)$ and ( $5 f$ ) are eliminated. Matching the core solution gives the conditions

$$
\begin{equation*}
\phi_{f} \rightarrow \phi_{c}(a, \theta), \quad F_{f} \rightarrow z p_{c}(a, \theta) \quad \text { as } \quad \xi \rightarrow-\infty \tag{9a,b}
\end{equation*}
$$

so that $(8 a)$ can be replaced by $F_{f}(\xi, \theta, 1)=p_{c}(a, \theta) . F_{f}$ and $\phi_{f}$ are odd and even functions of $z$, respectively. In the next Section, we present solutions for a specific distribution of the heat flux into the free surface.

The present neglect of convective heat transfer everywhere, inertial effects everywhere and viscous effects in the core assumes that the respective parameters $P e H a^{-1 / 4}, N^{-1}$ $H a^{3 / 2}$ and $H a^{-1 / 2}$ are small (Morthland \& Walker 1997). As an example, we consider the properties of molten silicon (Sabhapathy \& Salcudean 1991), a floating-zone axial length of 1 cm , and a temperature difference along the free surface of 15 K (Croll et al. 1994), so that $H a=207 B, N=81.83 B^{3}$ and $P e=6.79 B^{-1}$. For the $B=0.5$ T used by Croll et al. (1994), $P e H a^{-1 / 4}=4.257, N^{-1} H a^{3 / 2}=103$, and $H a^{-1 / 2}=0.1$. For this case,
convective heat transfer and inertial effects are clearly not negligible, and the present assumptions are not appropriate. Indeed the experiments of Croll et al. (1994) showed that an instability leads to a periodic flow which produces striations in the part of the crystal adjacent to the free-surface layer. Smith \& Davis (1983) showed that such an instability involves a coupling of convective heat transfer and inertial effects which produces hydrothermal waves propagating around the floating zone in the azimuthal direction. In order to eliminate these undesirable striations, researchers at the NASA Marshall Space Flight Center and at the University of Freiburg are collaborating to grow silicon crystals with the same floating-zone process used by Croll et al. (1994), but with $B=5 \mathrm{~T}$. For this magnetic flux density, the present assumptions are certainly appropriate. For these terrestrial experiments, the deviation from a cylindrical free surface will be small because the radius of the floating zone will be small. The model presented in this paper should help explain the results of these planned experiments.

All of the orders of magnitude in $H a^{-1 / 2}$ follow from our characteristic melt velocity $U$, which was chosen to give $O(1)$ dimensionless volumetric flow rates, i.e. flow rates which remain bounded and non-zero as $H a \rightarrow \infty$. The two temperature gradients driving the flow are the $\partial T / \partial \theta$ and $\partial T / \partial z$ in $(3 b, c)$. Since $\partial / \partial \theta$ and $\partial / \partial z$ are $O(1)$, while $\partial / \partial r$ is $O\left(H a^{1 / 2}\right)$ in the free-surface layer, (3c) implies that $v_{z}$ is always $O\left(H a^{1 / 2}\right)$ inside this layer, and $(3 b)$ implies that $v_{\theta}$ is $O\left(H a^{1 / 2}\right)$ inside this layer when $\partial T / \partial \theta$ is not zero. Since these large velocities are tangential velocities inside a layer with an $O\left(\mathrm{Ha}^{-1 / 2}\right)$ thickness, they represent $O(1)$ dimensionless flow rates. The axisymmetric flow is entirely confined to the free-surface layer, but any deviation from axisymmetry requires that the flow circuit be completed across the core, which implies $O(1)$ core velocities. The electric current arises from the large velocities in the free-surface layer, and each component of $\boldsymbol{j}$ in this layer is $O\left(H a^{-1 / 2}\right)$ smaller than the corresponding component of $\boldsymbol{v}$. The $O\left(H a^{-1 / 2}\right)$ current across the core arises from the need to complete the electrical circuit for the free-surface-layer currents.

## 3. Axisymmetric and non-axisymmetric solutions

The derivatives of $T(a, \theta, z)$ in $(7 a)$ and $(7 b)$ are the only inhomogeneous terms in the linear problem (6)-(9). Since the Fourier components in $\theta$ are decoupled, we can illustrate the effects of a non-axisymmetric heat flux with only the first two Fourier components, namely 1 and $\cos \theta$. For simplicity, we assume that the axial variation of the heat flux is given by $\cos \left(\frac{1}{2} \pi z\right)$, so that the separation-of-variables solution for $T$ has only one term. The boundary conditions on $T$ are

$$
\left.\begin{array}{rlrl}
\frac{\partial T}{\partial r} & =\cos \left(\frac{1}{2} \pi z\right)[1+\lambda \cos \theta] & & \text { at } \quad r
\end{array}\right)
$$

where the parameter $\lambda$ reflects the relative deviation from axisymmetry, i.e. the dimensional heat flux at $z=0$ varies from a maximum of $(1+\lambda) q$ at $\theta=0$ to a minimum of $(1-\lambda) q$ at $\theta= \pm \pi$, while $(10 b)$ reflects the fact that $T^{*}=T_{s}$ at the melting feed-rod surface and at the solidifying crystal surface. The solution for $T$ is

$$
\begin{equation*}
T=\cos \left(\frac{1}{2} \pi z\right)\left\{\frac{2}{\pi} I_{0}\left(\frac{1}{2} \pi r\right)\left[I_{1}\left(\frac{1}{2} \pi a\right)\right]^{-1}+\lambda \cos \theta I_{1}\left(\frac{1}{2} \pi r\right)\left[\frac{1}{2} \pi I_{0}\left(\frac{1}{2} \pi a\right)-a^{-1} I_{1}\left(\frac{1}{2} \pi a\right)\right]^{-1}\right\} \tag{11}
\end{equation*}
$$

where $I_{0}$ and $I_{1}$ are the modified Bessel functions of the first kind and zeroth or first order.

In both the core and the free-surface layer, $p, v_{r}, v_{z}, j_{\theta}$ and $F_{f}$ have the form $p=p_{a}+\lambda \cos \theta p_{n}$, while $\phi, v_{\theta}, j_{r}$ and $j_{z}$ have the form $\phi=\lambda \sin \theta \phi_{n}$, where the subscript $a$ denotes the axisymmetric melt motion with $\phi=v_{\theta}=j_{r}=j_{z}=0$, the subscript $n$ denotes the non-axisymmetric melt motion which is superimposed on the axisymmetric one, and variables with the subscript $a$ or $n$ are functions of $r$ in the core and of $\xi$ and $z$ in the free-surface layer.

For the axisymmetric flow, $\phi_{c a}=p_{c a}=0$, so that all the core variables are zero. Indeed, it is easy to show that all the core variables are zero to all order in Ha for the axisymmetric flow. In the free-surface layer, the separation-of-variables solution for $F_{f a}$ is

$$
\begin{align*}
F_{f a}=- & \pi^{-2} I_{0}\left(\frac{1}{2} \pi a\right)\left[I_{1}\left(\frac{1}{2} \pi a\right)\right]^{-1} \\
& \times \sum_{k=1}^{\infty}(-1)^{k} \gamma_{k}^{-1}\left(k^{2}-\frac{1}{4}\right)^{-1} \sin (k \pi z) \exp \left(\gamma_{k} \xi\right)\left[\sin \left(\gamma_{k} \xi\right)-\cos \left(\gamma_{k} \xi\right)\right] \tag{12}
\end{align*}
$$

where $\gamma_{k}=\left(\frac{1}{2} k \pi\right)^{1 / 2}$.
For the non-axisymmetric flow, the core solution is $\phi_{c n}=C_{1} r$ and $p_{c n}=C_{2} r$, where the constants $C_{1}$ and $C_{2}$ will be determined in the solution for the free-surface layer. In Cartesian coordinates with the $x$ - and $y$-axes parallel to the $\theta=0$ and $\theta=\frac{1}{2} \pi$ radii, respectively, (5) gives

$$
\begin{equation*}
v_{x}=-C_{1} \lambda, \quad v_{y}=0, \quad j_{x}=0, \quad j_{y}=C_{2} \lambda H a^{-1 / 2} \tag{13a-d}
\end{equation*}
$$

in the core, where $(13 a)$ and $(13 b)$ neglect $O\left(H a^{-1 / 2}\right)$ terms, while $(13 c)$ and $(13 d)$ neglect $O\left(\mathrm{Ha}^{-1}\right)$ terms. Since $C_{1}$ and $C_{2}$ both turn out to be negative, there is a uniform $O(1)$ velocity across the core from the cold side for $|\theta|>\frac{1}{2} \pi$ to the hot side for $|\theta|<\frac{1}{2} \pi$, and this flow drives a uniform $O\left(H a^{-1 / 2}\right)$ electric current from $0<\theta<\pi$ to $-\pi<\theta<0$. The uniformity of the core velocity and current follows from only including $\cos \theta$ - the $\cos 2 \theta$ term would involve a non-uniform core velocity from $\theta= \pm \frac{1}{2} \pi$ to $\theta=0$ and $\theta=\pi$, etc.

In the free-surface layer, $\phi_{f n}$ and $F_{f n}$ are governed by $(6 h)$ and $(6 i)$. In the freesurface conditions (7), the right-hand sides of $(7 a)$ and $(7 b)$ are replaced by

$$
\begin{equation*}
\frac{Q}{a} \cos \left(\frac{1}{2} \pi z\right), \quad \frac{1}{2} \pi Q \sin \left(\frac{1}{2} \pi z\right) \tag{14a,b}
\end{equation*}
$$

respectively, where

$$
\begin{equation*}
Q=I_{1}\left(\frac{1}{2} \pi a\right)\left[\frac{1}{2} \pi I_{0}\left(\frac{1}{2} \pi a\right)-a^{-1} I_{1}\left(\frac{1}{2} \pi a\right)\right]^{-1} \tag{14c}
\end{equation*}
$$

while the $\partial / \partial \theta$ in $(7 c)$ and $(7 d)$ is replaced by +1 and -1 , respectively. $\phi_{f n}$ satisfies (8b), and
while (9) become

$$
\begin{equation*}
F_{f n}=C_{2} a \quad \text { at } \quad z=1 \tag{15}
\end{equation*}
$$

$$
\begin{equation*}
\phi_{f n} \rightarrow C_{1} a, \quad F_{f n} \rightarrow C_{2} a z \quad \text { as } \quad \xi \rightarrow-\infty \tag{16a,b}
\end{equation*}
$$

The separation-of-variables solution for $(6 i),(7 b)$ with $(14 b),(15)$ and $(16 b)$ is

$$
\begin{align*}
F_{f n}=C_{2} a z+\sum_{k=1}^{\infty} \sin (k \pi z) \exp \left(\gamma_{k} \xi\right)\left\{A_{k}\right. & {\left[\sin \left(\gamma_{k} \xi\right)+\cos \left(\gamma_{k} \xi\right)\right] } \\
& \left.+Q(-1)^{k}\left[\pi \gamma_{k}\left(k^{2}-\frac{1}{4}\right)\right]^{-1} \cos \left(\gamma_{k} \xi\right)\right\} \tag{17}
\end{align*}
$$

where the coefficients $A_{k}$ will be determined by $(7 c)$ and ( $7 d$ ). For $\phi_{f n},(8 b)$ precludes a separation-of-variables solution, so we used a Fourier sine transform (Walker et al. 1972) to solve $(6 h),(7 a)$ with $(14 a)$, and $(8 b)$, and excluding exponential growth,

$$
\begin{align*}
\phi_{f n}(\xi, z) & =\frac{1}{2} \int_{-1}^{z}\left[\frac{Q}{a} \cos \left(\frac{1}{2} \pi z^{*}\right)+\frac{\partial \phi_{f n}}{\partial z}\left(0, z^{*}\right)\right] \operatorname{erf}\left[\frac{1}{2} \xi\left(z-z^{*}\right)^{-1 / 2}\right] \mathrm{d} z^{*} \\
& +\frac{1}{2} \int_{z}^{1}\left[\frac{Q}{a} \cos \left(\frac{1}{2} \pi z^{*}\right)-\frac{\partial \phi_{f n}}{\partial z}\left(0, z^{*}\right)\right] \operatorname{erf}\left[\frac{1}{2} \xi\left(z^{*}-z\right)^{-1 / 2}\right] \mathrm{d} z^{*}+\phi_{f n}(0, z) \tag{18}
\end{align*}
$$

The values of $\phi_{f n}(0, z)$ will also be determined by $(7 c)$ and $(7 d)$.
$C_{1}$ is determined by (16a) and (18):

$$
\begin{equation*}
C_{1}=a^{-1} \phi_{f n}(0,+1)-2 \pi^{-1} a^{-2} Q \tag{19}
\end{equation*}
$$

Equation (18) cannot be introduced directly into ( $7 d$ ) because the integrand at $\xi=0$ would be too singular at $z^{*}=z$, so that we integrated (18) by parts with respect to $z^{*}$ before differentiating thrice with respect to $\xi$ and setting $\xi=0$ for (7d). With (17) and (18), (7d) becomes a singular Fredholm integral equation for the values of $\partial^{2} \phi_{f n} / \partial z^{2}\left(0, z^{*}\right)$, and also involves a Fourier series with the coefficients $A_{k}$. The series in $(7 d)$ involves $\cos (k \pi z)$, beginning with $k=1$, so that the integral of (7d) from $z=0$ to $z=1$ gives

$$
\begin{equation*}
C_{2}=\pi^{-1 / 2} \int_{-1}^{1}\left[\frac{\pi Q}{2 a} \sin \left(\frac{1}{2} \pi z^{*}\right)-\frac{\partial^{2} \phi_{f n}}{\partial z^{2}}\left(0, z^{*}\right)\right]\left(1-z^{*}\right)^{1 / 2} \mathrm{~d} z^{*}+\left(\frac{2}{\pi}\right)^{1 / 2} \frac{\partial \phi_{f n}}{\partial z}(0,+1) \tag{20}
\end{equation*}
$$

We introduced (17) and (18) into (7c), multiplied by $\cos (m \pi z)$, and integrated from $z=0$ to $z=1$. For $m=0,(7 c)$ gives

$$
\begin{equation*}
\int_{0}^{1} \phi_{f n}(0, z) \mathrm{d} z=0 \tag{21}
\end{equation*}
$$

so that the values of $\phi_{f n}(0, z)$ and $\partial \phi_{f n} / \partial z(0, z)$ are easy to obtain from the values of $\partial^{2} \phi_{f n} / \partial z^{2}(0, z)$. For $m=1,2,3, \ldots,(7 c)$ gives

$$
\begin{equation*}
\int_{0}^{1} \frac{\partial^{2} \phi_{f n}}{\partial z^{2}}\left(0, z^{*}\right)\left[(-1)^{m}-\cos \left(m \pi z^{*}\right)\right] \mathrm{d} z^{*}+a \pi^{3} m^{3} \gamma_{m} A_{m}=-\frac{1}{2} a Q(-1)^{m} \pi^{2} m^{3}\left(m^{2}-\frac{1}{4}\right)^{-1} \tag{22}
\end{equation*}
$$

Equations (7d) and (22) are a pair of equations for $\partial^{2} \phi_{f n} / \partial z^{2}\left(0, z^{*}\right)$ and $A_{k}$. We divided the interval $0 \leqslant z \leqslant 1$ into $N Z$ segments, with the ends of the segments at the Gauss-Lobatto points, $z_{n}=\cos (n \pi / 2 N Z)$ for $n=0$ to $N Z$, so that the segments are short and long near $z=1$ and $z=0$ where the gradient of $\partial^{2} \phi_{f n} / \partial z^{2}\left(0, z^{*}\right)$ is large and small, respectively. We assumed that the value of $\partial^{2} \phi_{f n} / \partial z^{2}\left(0, z^{*}\right)$ is constant over each segment, giving $N Z$ discrete unknown values of this function. Equation (7d) was evaluated at the centre of each segment giving $N Z$ equations for the $N Z$ unknown values of $\partial^{2} \phi_{f n} / \partial z^{2}\left(0, z^{*}\right)$ and for $A_{k}$. The Fourier series in $(7 d)$ was truncated at $k=N A$ and (22) was used for $m=1$ to $N A$, giving a total of $(N Z+N A)$ simultaneous linear algebraic equations for the $(N Z+N A)$ unknown. Varying $N Z$ and $N A$ indicated that $N Z=N A=40$ gives excellent results. The values of the free-surface-layer variables are given by $(6 a-g)$, (17) truncated at $k=N A$, and (18) with the constant values of $\partial^{2} \phi_{f n} / \partial z^{2}\left(0, z^{*}\right)$ for each segment; while $C_{1}$ and $C_{2}$ are given by (19) and (20).

## 4. Results

Here we only present results for $a=1$. For the axisymmetric flow inside the freesurface layer, there is a stream function, but the contours of $v_{r f a}$ and $v_{z f a}$ in figure 2 are more useful than the streamlines for comparing the axisymmetric and non-


Figure 2. Contours of the velocity components for the axisymmetric flow inside the free-surface layer. (a) $v_{r f a}=-0.2 n$ for $n=1$ to 5 and $v_{r f a}=0.05 n$ for $n=1$ to 6 . (b) $v_{z f a}=-0.02 n$ for $n=1$ to 5 and $v_{z f a}=0.1 n$ for $n=1$ to 5 .
axisymmetric flows. In figure 2 , the velocity differences between adjacent contours are different for positive and negative values. Here $-1.26<v_{r f a}<0.341$, and $-0.118<v_{z f a}<0.561$. For the axisymmetric flow, the melt near the free surface flows toward each solid-liquid interface, turns to flow radially inward with a large velocity near the interface, flows back toward $z=0$ for $\xi<-0.7$ and then flows radially outward toward the free surface for $|z|<0.6$. These results agree with the axisymmetric results presented by Morthland \& Walker (1997).

While $v_{r f a}$ and $v_{z f a}$ are both zero at $\xi=0$ and $z=1$, figures $2(a)$ and $2(b)$ show that $\partial v_{r f a} / \partial \xi$ and $\partial v_{z f a} / \partial z$ have singularities at this corner. These singularities arise because $v_{z f a}=0$ at $z=1$ for all $\xi$, while $\partial v_{z f a} / \partial \xi$ at $\xi=0$ approaches its maximum value as $z \rightarrow 1$. The solution of the parabolic equation ( $6 i$ ) which satisfies these incompatible boundary conditions has the local behaviour

$$
\begin{equation*}
\frac{\partial v_{z f a}}{\partial \xi} \approx I_{0}\left(\frac{1}{2} \pi a\right)\left[I_{1}\left(\frac{1}{2} \pi a\right)\right]^{-1}\left\{1+\operatorname{erf}\left[\frac{\xi}{2(1-z)^{1 / 2}}\right]\right\} \tag{23}
\end{equation*}
$$

For the corner region (cr) in figure $1, \Delta r=O\left(H a^{-1}\right), \Delta z=O\left(H a^{-1}\right)$, and the governing equation is elliptic. The corner-region solution matches the singularities in the free-surface-layer velocity gradients at $\xi=0$ and $z=1$. The axial temperature gradient accelerates the flow along the free surface from the plane of symmetry at $z=0$ toward the solid surface at $z=1$. In the free-surface layer, the viscous momentum diffusion in the $z$-direction is negligible, so that nothing decelerates the flow until it is very close to the solid surface. Very near $z=1$, the flow abruptly turns radially inward, creating an abrupt decrease in $v_{r f a}$ from zero as $\xi$ decreases from zero. The infinite velocity gradients are resolved by the smaller scales of the corner region where all viscous effects are important. As always, there are no infinite velocity gradients at the physical scale of the viscous diffusion length, which is $H a^{-1}$ here, but there appear to be infinite velocity gradients when we study scales which are much larger than the viscous diffusion length.

For the non-axisymmetric flow, $C_{1}=-0.388$ and $C_{2}=-0.268$. The contours of $v_{r f n}, v_{\theta f n}$ and $v_{z f n}$ are presented in figure 3. Again there are singularities in the gradients of $v_{r f n}$ and $v_{z f n}$. In addition there are new singularities in $j_{r f n}$ and $j_{z f n}$ at $\xi=0$ and $z=1$. The total radial electric current inside the intersection region (i) in figure 1 at any value of $\xi$ is proportional to the local value of $v_{\theta f n}$ at $z=1$. Figure $3(b)$ shows that $v_{\theta f n}$ is not zero at $\xi=0$ and $z=1$, so that there is a non-zero radial electric current from the intersection region to the corner region. Continuity of electric current requires that this current in turn enter the free-surface layer as an apparent current source at $\xi=0$ and $z=1$. Indeed this current flows out of the corner region and into the freesurface layer along the parabolas defined by $\xi /(1-z)^{1 / 2}=$ constant.

Here $-0.723<v_{r f n}<0.502,0<v_{\theta f n}<0.539$, and $-0.0715<v_{z f n}<0.351$. The values of $v_{r f n}(\xi, z)$ and $v_{z f n}(\xi, z)$ are multiplied by $\cos \theta$, while the values of $v_{\theta f n}$ are multiplied by $\sin \theta$. The non-axisymmetric flow consists of a planar flow in $\theta=$ constant planes and a nearly planar flow which only moves slightly across $z=$ constant planes. The flow in $\theta=$ constant planes is confined to the free-surface layer and increases or decreases the axisymmetric flow on the hot side for $|\theta|<\frac{1}{2} \pi$ or on the cold side for $|\theta|>\frac{1}{2} \pi$, respectively. Most of $v_{z f n}$ in figure $3(c)$ is in this planar flow. The maximum values of $v_{z f a}$ and $v_{z f n}$ both occur at $\xi=0$ near $z=0.7$, so that the maximum axial-free-surface velocity at each azimuthal position is $(0.561+0.351 \lambda \cos \theta)$.

The other part of the non-axisymmetric flow consists of the uniform velocity $v_{x}=0.388 \lambda$ across the core from the cold side to the hot side and an azimuthal velocity inside the free-surface layer from the hot side to the cold side. In figure $3(b) v_{\theta f n}$ is the


Figure 3. Contours of the velocity components for the non-axisymmetric flow inside the free-surface layer. (a) $v_{r f n}=0.1 n$ for $n=-6$ to 5 . (b) $v_{\theta f n}=0.1 n$ for $n=1$ to 5 . (c) $v_{z f n}=-0.02 n$ for $n=1$ to 3 and $v_{z f n}=0.1 n$ for $n=0$ to 3 .
azimuthal velocity inside the free-surface layer and is nearly uniform in $z$, like the core velocity. The integral of $v_{\theta f n}$ from $\xi=-\infty$ to $\xi=0$ varies from 0.376 at $z=0$ to 0.408 at $z=1$, so that a small part of the $v_{z f n}$ in figure $3(c)$ provides an axial redistribution between the uniform core flow and the azimuthal flow inside the free-surface layer which is slightly stronger near the liquid-solid interfaces. In figure 3 (a) $v_{r f n}$ represents a superposition of the two parts of the non-axisymmetric flow. For the part in $\theta=$ constant planes, $v_{r f n}$ is positive and negative near $z=0$ and $z=1$, respectively. For the part which nearly lies in $z=$ constant planes, $v_{r f n}$ decreases from 0.388 at $\xi=-\infty$ to zero at $\xi=0$.

## 5. Conclusions

The thermocapillary convection in a cylindrical floating zone with a strong uniform axial magnetic field and with an axisymmetric heat flux into the free surface represents a special case in which the strong electromagnetic suppression of the motion completely eliminates all melt motion in the central core region, leaving only the circulation in the azimuthal planes inside a thin boundary layer adjacent to the free surface. If there is a deviation from axisymmetry in the heat flux, the azimuthal variation of the temperature around the free surface drives an azimuthal velocity inside the free-surface layer from the hot side to the cold side, and the circulation is completed by a velocity across the central core of the melt from the cold side to the hot side. This transverse flow across the entire face of the growing crystal could produce a variation of the dopant concentration across each cross-section of the crystal or lateral macrosegregation.

We can expect the transverse core flow driven by a deviation from axisymmetry in the heat flux to affect the distribution of a dopant in the crystal when the masstransport Péclet number based on the core velocity is greater than 1, i.e.

$$
\begin{equation*}
P e_{m}=\frac{\left(-C_{1} \lambda U\right) L}{D}>1 \tag{24}
\end{equation*}
$$

where $D$ is the diffusion coefficient for the dopant in the molten semiconductor. Using the properties of molten silicon, a zone length of 1.0 cm , a free-surface temperature difference of $15 \mathrm{~K}, B=5.0 \mathrm{~T}$ and the typical value $D=10^{-8} \mathrm{~m}^{2} \mathrm{~s}^{-1}$, (24) implies a significant effect for $\lambda>0.0089$. Therefore we can expect that even a small deviation from axisymmetry will have a significant effect on the dopant distribution.

Here we have only considered a relative deviation from an axisymmetric heat flux given by $\lambda \cos \theta$, i.e. the hottest and coldest azimuthal positions at $\theta=0$ and $\theta=\pi$, respectively. Certain floating-zone furnaces use two lamps placed diametrically opposite each other, so that the relative deviation from an axisymmetric heat flux will be given by $\lambda \cos (2 \theta)$, with the hottest positions at $\theta=0, \pi$ and the coldest positions at $\theta= \pm \frac{1}{2} \pi$. For this case, the $O(1)$ core $\phi$ is $C_{3} \lambda r^{2} \sin (2 \theta)$, so that the core velocities are

$$
\begin{equation*}
v_{x c}=-2 C_{3} \lambda x, \quad v_{y c}=2 C_{3} \lambda y \tag{25a,b}
\end{equation*}
$$

Since $C_{3}<0$, there is core flow from the coldest positions to the hottest positions in order to complete the flow circuit for the flows inside the free-surface layer.

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